

Homework 6 Solutions.

3-27 Complete the following table for H_2O :

T, °C	P, kPa	h, kJ / kg	x	Phase description
120.21	200	2045.8	0.7	<i>Saturated mixture</i>
140	361.53	1800	0.565	<i>Saturated mixture</i>
177.66	950	752.74	0.0	<i>Saturated liquid</i>
80	500	335.37	- - -	<i>Compressed liquid</i>
350.0	800	3162.2	- - -	<i>Superheated vapor</i>

3-28 Complete the following table for Refrigerant-134a:

T, °C	P, kPa	v, m³ / kg	Phase description
-8	320	0.0007569	<i>Compressed liquid</i>
30	770.64	0.015	<i>Saturated mixture</i>
-12.73	180	0.11041	Saturated vapor
80	600	0.044710	<i>Superheated vapor</i>

3-88 The specific volume of steam is to be determined using the ideal gas relation, the compressibility chart, and the steam tables. The errors involved in the first two approaches are also to be determined.

Properties The gas constant, the critical pressure, and the critical temperature of water are, from Table A-1,

$$R = 0.4615 \text{ kPa}\cdot\text{m}^3/\text{kg}\cdot\text{K}, \quad T_{cr} = 647.1 \text{ K}, \quad P_{cr} = 22.06 \text{ MPa}$$

Analysis (a) From the ideal gas equation of state,

$$v = \frac{RT}{P} = \frac{(0.4615 \text{ kPa}\cdot\text{m}^3/\text{kg}\cdot\text{K})(673 \text{ K})}{(10,000 \text{ kPa})} = \mathbf{0.03106 \text{ m}^3/\text{kg} \text{ (17.6\% error)}}$$

(b) From the compressibility chart (Fig. A-15),

H_2O 10 MPa 100°C

$$P_R = \frac{P}{P_{cr}} = \frac{10 \text{ MPa}}{22.06 \text{ MPa}} = 0.453$$

$$T_R = \frac{T}{T_{cr}} = \frac{673 \text{ K}}{647.1 \text{ K}} = 1.04$$

$$Z = 0.84$$

Thus,

$$v = Zv_{\text{ideal}} = (0.84)(0.03106 \text{ m}^3/\text{kg}) = \mathbf{0.02609 \text{ m}^3/\text{kg} \text{ (1.2\% error)}}$$

(c) From the superheated steam table (Table A-6),

$$\left. \begin{array}{l} P = 10 \text{ MPa} \\ T = 400^\circ\text{C} \end{array} \right\} v = \mathbf{0.02644 \text{ m}^3/\text{kg}}$$

4-25 A piston-cylinder device contains air gas at a specified state. The air undergoes a cycle with three processes. The boundary work for each process and the net work of the cycle are to be determined.

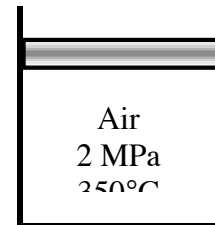
Properties The properties of air are $R = 0.287 \text{ kJ/kg}\cdot\text{K}$, $k = 1.4$ (Table A-2a).

Analysis For the isothermal expansion process:

$$V_1 = \frac{mRT}{P_1} = \frac{(0.15 \text{ kg})(0.287 \text{ kJ/kg}\cdot\text{K})(350 + 273 \text{ K})}{(2000 \text{ kPa})} = 0.01341 \text{ m}^3$$

$$V_2 = \frac{mRT}{P_2} = \frac{(0.15 \text{ kg})(0.287 \text{ kJ/kg}\cdot\text{K})(350 + 273 \text{ K})}{(500 \text{ kPa})} = 0.05364 \text{ m}^3$$

$$W_{b,1\rightarrow 2} = P_1 V_1 \ln \frac{V_2}{V_1} = (2000 \text{ kPa})(0.01341 \text{ m}^3) \ln \frac{0.05364 \text{ m}^3}{0.01341 \text{ m}^3} = \mathbf{37.18 \text{ kJ}}$$



For the polytropic compression process:

$$P_2 V_2^n = P_3 V_3^n \Rightarrow (500 \text{ kPa})(0.05364 \text{ m}^3)^{1.2} = (2000 \text{ kPa}) V_3^{1.2} \Rightarrow V_3 = 0.01690 \text{ m}^3$$

$$W_{b,2\rightarrow 3} = \frac{P_3 V_3 - P_2 V_2}{1 - n} = \frac{(2000 \text{ kPa})(0.01690 \text{ m}^3) - (500 \text{ kPa})(0.05364 \text{ m}^3)}{1 - 1.2} = \mathbf{-34.86 \text{ kJ}}$$

For the constant pressure compression process:

$$W_{b,3\rightarrow 1} = P_3 (V_1 - V_3) = (2000 \text{ kPa})(0.01341 - 0.01690) \text{ m}^3 = \mathbf{-6.97 \text{ kJ}}$$

The net work for the cycle is the sum of the works for each process

$$W_{\text{net}} = W_{b,1\rightarrow 2} + W_{b,2\rightarrow 3} + W_{b,3\rightarrow 1} = 37.18 + (-34.86) + (-6.97) = \mathbf{-4.65 \text{ kJ}}$$

